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# Position Control of Servo Driven Ball Screw for Minimizing Backlash

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**ABSTRACT:** Backlash is a common but intractable problem in CNC machine tools, which may degrade the contouring accuracy significantly. A lot of work has been done to investigate the backlash error. However, the previous investigations about backlash error mainly focus on traditional CNC machine tools with semi-closed loops, i.e. the position feedback of feed drive is from the encoder of servo- motor. In these traditional machine tools, backlash error is ever-present and constant, which equals half width of backlash. To improve the machining accuracy, closed loops (the so-called full- closed loops) have been widely applied instead of the semi-closed loops. The ball screw drives are among the most commonly mechanisms used to provide motion inhigh speed machine tools. The most important factor that affects high speed positioning accuracy is the closed loop bandwidth, which in turn is affected by the structural vibration modes. In recent years, newer strategies have emerged achieving higher control bandwidth, but requiring higher order plan models as well as a better understanding of the system dynamics.

**KEYWORDS:** Backlash; Ballscrew, Positioning error, PID controller.

### I. INTRODUCTION

Backlash is one of the most commonly encountered nonlinear phenomena in feed drives, which degrades the contouring accuracy of machine tools. Its performances on positioning system or speed control depend on the motion accuracy and characteristics of mechanisms and the controllers. [1] The role of the controller is to overcome the mechanical limitations and to utilize their characteristics for high positioning performance. Mechanical elements used in precision positioning systems, such as gearand actuators often have the characteristics, which maydegrade the positioning performance, for example, friction brushes and/or bearings with mechanical contact in motors. Friction will cause steady-state and tracking errors, limit cycles that can slow down of the mechanisms motions. [2]

The control of systems with backlash has been the subject of study since 1940s. Linear controllers have been investigated, including P-, PI-, and PID-controllers, high-order linear controllers, state feedback controllers, and observer based controllers. The main analytical tool to describe the backlash has been the describing function technique. The preload, i.e. an approximate inverse of the backlash, has often been suggested as a backlash remedy, both in a non-adaptive and an adaptive setting. [8] Other non-linear controllers have also been proposed, including fuzzy controllers and switched linear controllers. In this thesis the PID controller is used for controlling the backlash in system model because it is very effective in controlling the error & easy to tune thus providing the desired outputs. Since many control systems using PID control have proved satisfactory, it still has a wide range of applications in industrial control. Since many process plants controlled by PID controllers have similar dynamics it has been found possible to set satisfactory controller parameters from less plant information than a complete mathematical model. [4]

### **II. RELATED WORK**

Control valves are subject to wear. After some time in operation, this wear results in friction and backlash that deteriorates the control performance. Therefore, valves have been identified as the major source of problems at the loop



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level in process control [,2]. Valves with a high level of static friction (station) results in stick-slip motion that causes the control loops to oscillate. As the amount of friction increases, so does the backlash in the linkage mechanism in the positioner and actuator of the valve. The backlash adds a time delay to the control loop which deteriorates the control. In [2], it is reported that a backlash of 10% increases the peak error at load disturbances with 50% and the integrated absolute error (IAE) with 100%. These figures are dependent on the magnitude of the load disturbances, but simulation studies presented later in this paper verify them. Since control loops in process control applications often are coupled to surrounding control loops, there is also a risk that the disturbances caused by backlash in one loop will propagate to other loops. When the station or backlash becomes large, the valve should, of course, be repaired or replaced. However, this can normally not be done without interrupting the process. For this reason, and other economic reasons, it is of interest to try to keep the valve running for as long time as possible. Station can be compensated for using the method presented in [4]. Backlash is easier to compensate for, since it is an invertible nonlinearity. This will be discussed further in Section 3 in this paper. Even though the problems caused by station and backlash are severe; they are often not discovered by operators in process control plants. The main reason is that the reduction of personnel has resulted in a situation where each operator simply has too many loops to supervise. For this reason, the research on procedures for automatic performance monitoring has been very active in the last decade. The industrial use of these procedures has also increased rapidly in recent years. Good surveys of performance monitoring procedures are given in [5-8]. There are several methods suggested for detecting control loops with stiction, e.g. [9]. However, no efficient procedure to detect backlash has been presented so far, but this paper provides such a procedure. In the next section, a description and an analysis of backlash is presented. Section 3 gives some methods to compensate for backlash. The main section of this papera typical structure of a PID control system is shown in Fig 1, where it can be seen thatin a PID controller, the error signal e(t) is used to generate the proportional, integral, and derivative actions, with the resulting signals weighted and summed to form the control signal u(t) applied to the plant model. A mathematical description of the PID controller is

 $\mathbf{u}(t) = K_p \left[ \mathbf{e}(t) + \frac{1}{T_i} \int_0^t \mathbf{e}(\tau) d\tau + T_d \frac{d\mathbf{e}(t)}{dt} \right]$ (1)

where u(t) is the input signal to the plant model, the error signal e(t) is defined as e(t) = r(t) - y(t), and r(t) is the reference input signal.

#### **III. PID TUNING METHODS**

A very useful empirical tuning formula was proposed by Ziegler and Nichols in early 1942. The tuning formula is obtained when the plant model is given by a first-order plus dead time (FOPDT) which can be expressed by

$$G(s) = \frac{\kappa}{1+sT}e^{-sT}$$

In real-time process control systems, a large variety of plants can be approximately modeled by (2). If the system model cannot be physically derived, experiments can be performed to extract the parameters for the approximate model (2). For instance, if thestep response of the plant model can be measured through an experiment, the output signalcan be recorded as sketched in Fig. 6.7(a), from which the parameters of k, L, and T (ora, where a = kL/T) can be extracted by the simple approach shown. More sophisticated curve fitting approaches can also be used. With L and a, the Ziegler–Nichols formula in Table 1 can be used to get the controller parameters.

Controller Type	$K_p T_i T_d T_p$			
Р	$0.5 K_u T_u$			
PI	$0.4K_u$	$0.8T_u$		$1.4T_{u}$
PID	$0.6K_u$	$0.5T_u$ 0.1	125 <i>T</i> <sub>u</sub>	0.85 <i>T</i> <sub>u</sub>

Table-1 Ziegler Nichols parameter



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The controller C has set point $y_{sp}$  and process output y as inputs, and control signal u as output. The controller output u is not the input to process P, but it goes through a backlash that gives the true process input ub. The function of the backlash, where the dead band caused by the backlash is denoted d. When the control signal u is reversed, the process input ubremainsconstant until u has passed the dead band d. The describing function YN of a backlash is

$$\operatorname{Re}Y_{N}\left(a\right) = \frac{1}{\pi} \left(\frac{\pi}{2} + \arcsin\left(1 - \frac{d}{a}\right) + \left(1 - \frac{d}{a}\right)\sqrt{\frac{d}{a}}\left(2 - \frac{d}{a}\right)\right)$$
$$\operatorname{Im}Y_{N}\left(a\right) = -\frac{d}{\pi a}\left(2 - \frac{d}{a}\right)$$
(3)



Fig. 1. Block diagram of a control loop with backlash.

The controller C has inputs setpoint  $y_{sp}$  and process output y. The controller output u goes through the backlash and is modified to  $u_b$  before it enters the input of process P.



Fig. 2. The output  $u_b$  from a backlash with input u. The dead band of the backlash is d.



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Fig. 3. The negative inverse of the describing function of a backlash (solid line) and the Nyquist plots of the loop transfer functions obtained when the processes  $P1 = e_0.2s/(s(1 + 0.8s))$  (dashed line) and P2 = 1/(1 + s)4(dashed-dotted line) are controlled with PID controllers

where 'a' is the input amplitude and d is the backlash given in Fig. 2 [2]. The negative inverse of the describing function of the backlash is shown in Fig. 3. The figure shows also the Nyquist plots of two loop transfer functions obtained when an integrating and a stable process, respectively, are controlled by PID controllers. From this figure it can be concluded that backlash generates limit cycles when integrating processes are controlled by controllers with integral action. The figure also shows that backlash will normally not generate limit cycles when the process is stable, provided that the controller is well tuned. Since d is divided by a atevery position where it appears in (1), the shape of the describing function is independent of d. This has an interesting consequence. It means that the magnitude d of the backlash will influence the oscillation amplitude, but since the intersection with the Nyquistplot occurs at the same position, the oscillation period will remain the same independent of the magnitude of the backlash. Throughout this paper it is assumed that the controller C is a PID controller. This is mostly the case in practice. However, the results presented in this paper can quite easily be modified to other controllers having integral action The PID controller used in the following examples has the structure:

$$u(t) = K\left(-y_f(t) + \frac{1}{T_i} \int Y_{sp}(t) - y_f(t) dt - T_d \frac{dy_f(t)}{dt}\right)$$
(4)

#### **IV. MODELLING OF THE SYSTEM**

A transfer function of a system with backlash from the paper 1 is taken to build the system model with backlash. The backlash and noise is compensated by using PID controller . For this the PID controller is to be tuned by using tuning method called Ziegler –Nichols method. Using the Ziegler Nichols parameters given in the table thr gains of PID controller are determined & then PID controller is tuned. For calculating gains of controller first of  $allK_u, T_i, T_d$  these are ultimate point, integral time, derivative time is to be determined by using nyquist plot. By taking transfer function of the desired system the nyquist plot of that system is to be plotted which shows the value of  $K_u$  and  $T_u$ . An example of a stable process with backlash is given in the form of transfer function[2].

$$P(s) = \frac{1}{(1+s)^4}$$
(5)  
$$P(s) = s^4 + 4s^3 + 6s^2 + 4s + 1$$
(6)



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In the above transfer function external backlash of 5% i.e 0.05 is added & also noise is added and then PID controller is used to compensate the error. For the tuning the PID controller ultimate point  $K_u$  and ultimate time  $T_u$  is to be determined from nyquist plot.



Nyquist plot of the given transfer function

From the above Nyquist plot the  $K_p$ ,  $T_i$ ,  $T_d$  are obtained and from these  $K_p$ ,  $K_i$ ,  $K_d$  are obtained and using these parameters the PID controller is tunned. From the above plot  $K_u$  and  $T_u$  are obtained  $K_u$ =-1 / ultimate point which is the point at which the nyquist plot intersects the real axis, here it is -0.243 therefore  $K_u$ =-1/-0.243=4.115 and now  $T_u$ = 2Pi/ w here w is angular frequency of ultimate point which is w=-1.01 rad/sec, therefore  $T_u$ =2pi/-1.01=6.217 sec is obtained. The PID gains are calculated using these two parameters  $K_u$  and  $T_u$ .  $K_p$  which is proportional gain is calculated



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as  $K_p=0.6K_u$  similarly  $T_i$  and  $T_d$  are calculated.  $T_i=0.5T_u=3.1085$  sec and  $T_d=0.125T_u=0.777$  sec. From these parameters PID gains i.e  $K_p$ ,  $K_i$ , and  $K_d$  are calculated  $K_p=0.6K_u=2.469$ ,  $K_i=K_p/T_i=0.794$  and  $K_d=K_p*T_d=1.918$ .

### V. SIMULATION OF THE ABOVE TRANSFER FUNCTION.



Simulation of transfer functions of the system with backlash.



Simulation output.

The transfer function of the D.C motor is taken from (2) and Leadscrew equation is taken from (3) then backlash and external noise is added in it and then error is compensated using PID controller. The method mentioned above is used to calculate the tunning parameters.



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### Simulation of D.C motor and Leadscrew with backlash and noise.



#### Simulation output.

The output shows that the system remains stable in presence of backlash & external noise by using PID controller.

### VI. CONCLUSION

In this thesis a table driven system has been modeled. The system has been designed as a two masssystem consisting of a motor and a load connected via a ball screw consisting of backlash. In this analysis conventional PID controller is also studied with its advanced tuning methods in order to compensate the backlash error and achieve positioning accuracy of the sliding table driven by ball screw. The transient characteristicssuch as rise time, peak time, settling time also considered. In future we can improve the performance of motor by varying the parameters as well as introducing intelligent control system based on fuzzy or neuralnetwork to present system



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